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(54) Title: POLYMERIZATION PROCESS USING TERTIARY-AMYLPEROXY PIVALATE AS THE FREE RADICAL INITIATOR

(57) Abstract

Free radical polymerization of monomers in the presence of t-amylperoxy pivalate as the free radical initiator is described. Copolymers of maleic anhydride and a vinyl monomer, e.g. a C_1 - C_5 alkyl vinyl ether, and water soluble polyvinylpyrrolidone, are representative polymers prepared in accordance with the process of the invention.

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POLYMERIZATION PROCESS USING TERTIARY-AMYLPEROXY PIVALATE AS THE FREE RADICAL INITIATOR

BACKGROUND OF THE INVENTION

1. Field of the Invention

This invention relates to a process for making polymers, and, more particularly, to a polymerization process using t-amylperoxy pivalate as the free radical initiator.

2. Description of the Prior Art

Free radical initiators used in polymerization processes at elevated temperatures have included alkyl peresters, dialkyl peroxides, perketals, peroxydicarbonates, hydroperoxides, azo compounds and carbon-carbon labile compounds. Copolymerization also has been carried out at relatively low temperatures, e.g. room temperature, using a redox catalyst, such as, a combination of a redox catalyst and ascorbic acid, or, of a peroxydicarbonate and benzoin. It has been possible also to employ the polymerization initiator conjointly with a suitable accelerator, for example, an amine derived from a cyclic or phenyl structure, the amine being used by itself or together with an organic compound of a transition metal. Copolymerization also has been carried out with a mixture of different polymerization initiators having different decomposition temperatures.

The following compounds have been employed in free radical initiated polymerizations: acetyl cyclohexanesulfonyl peroxide, diacetyl peroxydicarbonate, dicyclohexyl peroxydicarbonate, di-2-ethylhexyl peroxydicarbonate, tert-butyl per[oxy]-neodecanoate, 2,2'-azobis(4-methoxy-2,4-dimethylvaleronitrile); tert-butylperoxy pivalate, dioctanoyl peroxide, dilauroyl peroxide, 2,2'-azobis-(2,4-dimethylvaleronitrile), tert-butylazo-2-cyanobutane; dibenzoyl peroxide, tert-butyl per[oxy]-2-ethylhexanoate, tert-butyl per[oxy]maleate, 2,2-azobis(isobutyronitrile); bis(tert-butylperoxy)cyclohexane, tert-butylperoxyisopropyl carbonate, tert-butyl per[oxy]acetate; 2,2-bis(tert-butylperoxy) butane, dicumyl peroxide, di-tert-amyl peroxide, di-tert-butyl peroxide, pinane hydroperoxide, cumene hydroperoxide, and tert-butyl hydroperoxide.

These polymerization initiators are used in amounts of about 0.05 to 10% by weight of the monomers, and, preferably about 0.1 to 5% by weight of an initiator is required.

t-Butylperoxy pivalate (TBPP) is a widely used free radical polymerization initiator: see U.S. patents 3,624,123; 3,887,528 and 4,237,257. TBPP undergoes thermal homolysis to produce t-butoxy and t-butyl free radicals.

Thermal Homolysis of TBPP

whereupon β -scission of the t-butoxy radical produces the methyl free radical:

$$CH_3$$
 CH_3
 CH_3
 CH_3
 CH_3
 CH_3
 CH_3
 CH_3
 CH_3
 CH_3

Thus, the active free radical species for initiation of free radical polymerization are:

Active Free Radical Species of TBPP

The methyl and t-butoxy free radicals, respectively, have high bond dissociation energies (BDE) of 104 and 105 kcal/mole. This means that these radicals can readily abstract a labile hydrogen atom from the polymer to convert an otherwise linear polymer into branched polymers which have lower water solubility and lower molecular weights than the linear polymers. In addition, the half-life of TBPP initiator, i.e. the time at a given temperature to effect a loss of one-half of the perester's active oxygen content, is a lengthy 24.6 hours at 50°C. Accordingly, TBPP requires a high reaction temperature, e.g. 60°-80°C., to carry out the polymerization within a reasonable period of time.

Accordingly, it is an object of this invention to provide polymerization processes using a free radical initiator whose thermal homolysis reaction provides free radicals which undergo rapid β -scission to produce active free radical species which are weak hydrogen abstractors, and, thus enable the formation of linear polymers having high degree of water solubility and high molecular weights.

SUMMARY OF THE INVENTION

A free radical initiated polymerization process is described herein in which at least one monomer is polymerized in the presence of t-amylperoxy pivalate as the free radical initiator. Representative polymerizations using the t-amylperoxy pivalate initiator of the invention include the copolymerization of maleic anhydride and a C_1 - C_5 alkyl vinyl ether to produce 1:1 alternating copolymers, and the homopolymerization of vinyl pyrrolidone to form high molecular weight polyvinyl pyrrolidone.

The polymerization processes of the invention are carried out at a faster reactivity rate, and at a lower temperature, than the same polymerizations using related free radical initiators. The process herein may provide linear polymers of high molecular weight, as contrasted to branched polymers of low molecular weight, formed with other initiators.

DETAILED DESCRIPTION OF THE INVENTION

In accordance with the invention, a free radical polymerization process is provided herein in which t-amylperoxy pivalate (TAPP) is used as the free radical polymerization initiator. TAPP undergoes thermal homolysis as follows:

Thermal Homolysis of TAPP

$$\begin{array}{c} \text{CH}_3 & \text{O} & \text{CH}_3 \\ \text{CH}_3 - \text{CH}_2 - \text{C} - \text{O} - \text{O} - \text{C} - \text{C} - \text{CH}_3 \\ \text{CH}_3 & \text{CH}_3 \end{array}$$

$$\begin{array}{c} \text{CH}_3 \\ \text{CH}_3 \text{CH}_2 - \text{C} - \text{O} \cdot \text{C} \\ \text{CH}_3 \end{array}$$

$$\begin{array}{c} \text{CH}_3 \\ \text{CH}_3 \end{array}$$

followed by eta -scission of the t-amyloxy radical:

$$CH_3CH_2$$
- $C-O$
 CH_3
 CH_3

Accordingly the active free radical species of TAPP are:

t-butyl radical

The ethyl and t-amyloxy free radical has a BDE of only 98 kcal/mole, and is therefore a relatively weak hydrogen abstractor. Thus, linear polymers can be provided using the TAPP initiator of the invention.

For example, polyvinylpyrrolidone (PVP) formed by free radical polymerization of vinyl pyrrolidone has several active hydrogen sites indicated by the asterisks for hydrogen abstraction, by active free radical species of TBPP

which would product branched PVP polymers:

whereas TAPP, having weak hydrogen abstractors can produce more nearly linear PVP polymers having increased water dissolution.

The invention will now be described by reference to the following examples.

Furthermore, it is known that lower molecular weight polymers are produced when high polymerization temperatures or long reaction periods are required. TAPP, as compared to TBPP, can effect completed polymerizations at lower temperatures, and/or with shorter reaction periods, it is possible also to produce higher molecular weight polymers than hitherfore achieved.

Suitably, the t-amylperoxy pivalate initiator of the invention may be used in free radical initiated polymerizations where at least one monomer is polymerizated in the presence of a free radical initiator. Representative free radical polymerizations include the preparation of maleic anhydride-based polymers, e.g. copolymerization of maleic anhydride with C_1 - C_5 alkyl vinyl ethers, with styrene, and/or with acrylic acid; the preparation of polyvinylpyrrolidone by the homopolymerization of vinyl pyrrolidone, and for other free radical polymerizations well known in the art.

The t-amylperoxy pivalate initiator is employed in these polymerizations in an amount of about 0.01 to 10% by wt. of the monomers, preferably about 0.1 to 5%.

The polymers produced using the TAPP initiator are characterized by being more water soluble (more linear, less branched), of controlled (lower) viscosity (higher molecular weight) and with less residual monomer (< 1000 ppm, higher purity, less toxic) than the same polymers made with other, even closely related free radical initiators.

The t-amylperoxy pivalate may be obtained from the Pennwalt Corp. under their commercial name of Lupersol 554M75, which is a 75% by wt. active solution in odorless mineral spirits.

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EXAMPLE 1

Preparation of Polyvinylpyrrolidone

A 2-liter reactor was provided with agitation, gas inlet, condenser, and thermocouple and was charged with 270 g. (2.3 moles) of non-stabilized vinyl pyrrolidone monomer, buffered with 0.27 g. of tetrasodium pyrophosphate and 1,080 g. of deionized water. The reactor was swept clean of oxygen by admitting nitrogen gas through the inlet Then the reactor was heated to 55°C. and 0.25 g. of t-amylperoxy pivalate was added (< 0.1% by wt. of vinyl pyrrolidone). The reaction was carried out at 56°-59°C. Then an additional 0.25 g. of TAPP was added for 5 hours. and the reaction continued for 2 hours. At the end of the reaction period, the reaction product included 21% solids with a residual monomer content of only 0.04%. polymer product in water was characterized by a K-value of 121; a Brookfield viscosity of 120,000 cps at 26°C. and excellent water dissolution.

EXAMPLE 2

Preparation of Copolymers of Maleic Acid and Methyl Vinyl Ether

A 1-liter pressure reactor was charged with 63.8 g. of methyl vinyl ether and 143 g. of acetone. A solution of 98 g. of maleic anhydride in 147 g. of acetone was prepared and charged into a syringe pump. The reactor was heated until the temperature of the charge reached 55°C. Then 0.94 g. of t-amylperoxy pivalate (1% by wt. of maleic anhydride) was introduced in 20 ml. of the maleic anhydride solution in one shot. Thereafter, the rest of

the solution was fed into the reactor continuously over a 4-hour period. Afterwards, the reaction mixture was held at 55°C. for an hour and the reactor was cooled to 25°-30°C. Excess methyl vinyl ether was removed and collected. The reaction product was discharged as a solution of maleic anhydride - methyl vinyl ether copolymer in acetone. The specific viscosity of the product at 25°C. was 0.38 as measured in 2-butanone (1% solution).

EXAMPLE 3

The procedure of Example 1 was followed to make PVP, using t-butylperoxy pivalate in place of t-amylperoxy pivalate. The product had a K-value of only 112; a residual monomer content of 0.14%, and relatively poor water dissolution.

EXAMPLE 4

The procedure of Example 2 was followed using t-butylperoxy pivalate. The specific viscosity of the copolymer was only 0.25.

While the invention has been described with particular reference to certain embodiments thereof, it will be understood that changes and modifications may be made which are within the skill of the art. Accordingly, it is intended to be limited by the appended claims only, in which:

WHAT IS CLAIMED IS:

- 1. A free radical initiated polymerization process which comprises effecting polymerization of at least one monomer in the presence of t-amylperoxy pivalate as the free radical initiator.
- 2. A polymerization process which comprises copolymerizing maleic anhydride and a C₁-C₅ alkyl vinyl ether in the presence of t-amylperoxy pivalate as a free radical initiator.
- 3. A polymerization process for making polyvinylpyrrolidone which comprises polymerizing vinyl pyrrolidone in the presence of t-amylperoxy pivalate as a free radical initiator.
- 4. A polymerization process according to claim 2 wherein the reaction temperature is about 55°-85°C.
- 5. A polymerization process according to claim 2 wherein the polymerization is carried out in a solvent.
- 6. A polymerization process according to claim 5 wherein said solvent is a ketone, ester, ether, aliphatic hydrocarbon, aromatic hydrocarbon, or aliphatic chlorinated hydrocarbon.

- 7. A polymerization process according to claim 6 wherein said solvent is acetone.
- 8. A polymerization process according to claim 6 wherein said initiator comprises about 1-10% by weight of maleic anhydride present.
- 9. A polymerization process according to claim 3 in which the reaction temperature is about 56°-59°C.
- 10. A polymerization process according to claim 9 wherein polymerization is carried out in water.
- 11. A polymerization process according to claim 10 wherein the PVP polymer product in water has a 21% solids content, a K-value of 121, a Brookfield viscosity of 120,000 cps at 26°C., and a residual monomer content of about 0.04% or less.
- 12. A polymerization process according to claim 3 wherein said initiator is present in an amount of about 0.1 to 10% by wt. of vinyl pyrrolidone monomer present.

- 13. A polymerization process according to claim 12 wherein the initiator level is about 0.5 to 2%.
- 14. A polyvinyl pyrrolidone composition in water at about 21% solids having a PVP K value of about 12, a Brookfield viscosity of 120,000 cps at 26°C., and a residual monomer content of about 0.04% or less.

		INTERNATIONAL	- SEARCH REPORT						
I. CLASSIFICATION OF SUBJECT MATTER (I and the subject of the subj									
IPC (5): C08F 4/28, 4/34, 26/10, 220/08									
U.S. CL. 526/227, 264, 317.1									
II. FIELDS SEARCHED									
Minimum Documentation Searched 7 Classification System									
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u.s.		526/227, 264, 317.1							
Documentation Searched other than Minimum Documentation									
to the Extent that such Documents are Included in the Fields Searched									
		ONSIDERED TO BE RELEVANT	·						
Calegory *	Citati	on of Document, 11 with indication, where a	opropriate, of the relevant passages 12	Relevant to Claim No. 13					
<u>X</u> Y	US, A 04 AP	, 4,818,794 (DENZING RIL 1989: See column	ER ET AL) 3, lines 38-39.	1 2, 4-8					
Y	US, A See t	, 4,613,483 (COHEN) he entire document.	23 SEPTEMBER 1986	2, 4-8					
Y	US, A See t	, 4,816,534 (NUBER E he entire document.	T AL) 28 MARCH 1989	3, 9-12					
			•						
* Special	categories	of cited documents: 10	·						
"A" docu	ment definic	o the general state of the second	"T" later document published after the or priority date and not in conflict cited to understood the original						
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	vale		"X" document of particular relevance	the claimed invention					
		may throw doubts on priority claim(s) or establish the publication date of another	involve an inventive step	cannot be considered to					
"O" docu	ment referris	special reason (as specified) ng to an oral disclosure, use, exhibition or	cannot be considered to involve a						
"P" docu	ment publist	and prior to the interesting to the	ments, such combination being of in the art.	primore other such docu-					
"å" document member of the same patent family									
IV. CERTIFICATION Date of the Actual Completion of the Actual Completi									
Date of the Actual Completion of the International Search 22 OCTOBER 1990 Date of Mailing of this International Search Report 2 A IAN 1991									
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International Searching Authority ISA/US			Thomas McDonald, Jr.						
			<u>. </u>	3					

3. No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to

4. As all searchable claims could be searched without effort justifying an additional fee, the International Searching Authority did not invite payment of any additional fee.

the invention first mentioned in the claims; it is covered by claim numbers:

☐ The additional search fees were accompanied by applicant's protest.
 ☐ No protest accompanied the payment of additional search fees.

Con't. from PCT/ISA/210 supplemental sheet (2).

**** Subclass 264.

The international application lacks unity of invention under PCT Rule 13 because of the following reason:

Inventions I and II do not form a single inventive concept because they are drawn to two mutually exclusive species of polymerization process and are thus different inventions (claim 1 is generic to both processes).